

Appl. No. 10/763,024
Atty. Docket No.: 2003B003/2
Amendment dated June 22, 2007
Reply to Office Action dated April 18, 2007

RECEIVED
CENTRAL FAX CENTER

JUN 22 2007

Amendments to the Claims:

This listing of claims will replace all prior versions and listing of claims in this application.

Listing of Claims:

1.-24. (Cancelled)

25. (Currently Amended) A process for producing one or more olefin products from a methanol feed stream in a reactor, the process comprising the steps of:

- (a) supplying the methanol feed stream to the reactor;
- (b) contacting the methanol feed stream with a molecular sieve catalyst composition in the reactor to produce an effluent stream;
- (c) heating high pressure steam with the effluent stream;
- (d) heating medium pressure steam with the effluent stream; and
- (e) recovering the one or more olefin products from the effluent stream, wherein the step of (e) recovering occurs after the step of (d) heating.

26. (Currently Amended) The process of claim 25, wherein the step of (c) heating comprises the steps of:

- (c-i) heating high pressure saturated steam with the effluent stream to produce high pressure superheated steam; and
- (c-ii) heating water with the effluent stream to produce the high pressure saturated steam, wherein the step of (c-i) heating occurs before the step of (c-ii) heating.

27. (Currently Amended) The process of claim 25, further comprising the step of:
[(g)] (f) heating the methanol feed stream with the effluent stream.

28. (Original) The process of claim 27, wherein the step of (c) heating occurs before the step of (d) heating.

Appl. No. 10/763,024
Atty. Docket No.: 2003B003/2
Amendment dated June 22, 2007
Reply to Office Action dated April 18, 2007

29. (Currently Amended) The process of claim 28, wherein the step of [(g)] (f) heating occurs after the step of (d) heating.

30-33. (Cancelled)

34. (Original) A process for producing one or more olefin products from methanol in a reactor, the process comprising the steps of:

- (a) supplying a methanol feed stream to the reactor;
- (b) contacting the methanol feed stream with a molecular sieve catalyst composition in the reactor and withdrawing an effluent stream having a first temperature;
- (c) cooling the effluent stream in no less than four stages to produce a cooled effluent stream, wherein each of the four stages decreases the effluent stream temperature by no less than 50°F (28°C) and wherein the effluent stream has a second temperature after the four stages that is at least 500°F (280°C) less than the first temperature.

35. (Original) The process of claim 34, wherein the four stages decreases the effluent stream temperature by no less than 75°F (42°C).

36. (Original) The process of claim 34, wherein the four stages decreases the effluent stream temperature by no less than 100°F (56°C).

37. (Original) The process of claim 34, wherein the four stages decreases the effluent stream temperature by no less than 125°F (69°C).

38. (Original) The process of claim 34, wherein the four stages decreases the effluent stream temperature by no less than 150°F (83°C).

Appl. No. 10/763,024
Atty. Docket No.: 2003B003/2
Amendment dated June 22, 2007
Reply to Office Action dated April 18, 2007

39. (Original) The process of claim 34, wherein the second temperature is at least 600°F (333°C).
40. (Original) The process of claim 34, wherein the second temperature is at least 700°F (389°C).
41. (Original) The process of claim 34, wherein the second temperature is at least 800°F (444°C).
42. (Original) The process of claim 34, wherein the second temperature is at least 900°F (500°C).